

SGF – wood based bio-crude®

KLAUS SCHÖFFEL CTO - SGF

Silva Green Fuel

- 100% subsidiary of Statkraft AS
- Owns and operates a demonstration plant at Tofte (Norway), with the aim of demonstrating HTL technology
- Development of a full-scale commercial plant is taking place in parallel
- 40 employees

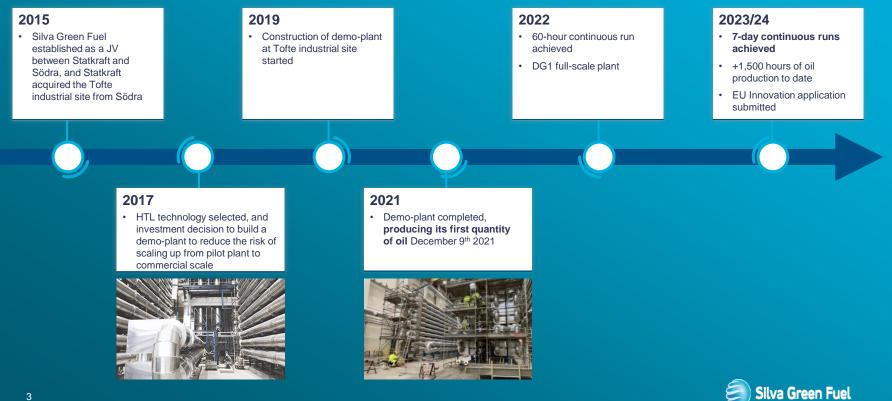
Our Ambition:

Silva Green Fuel to become a leading producer of bio-crude oil based on HTL technology

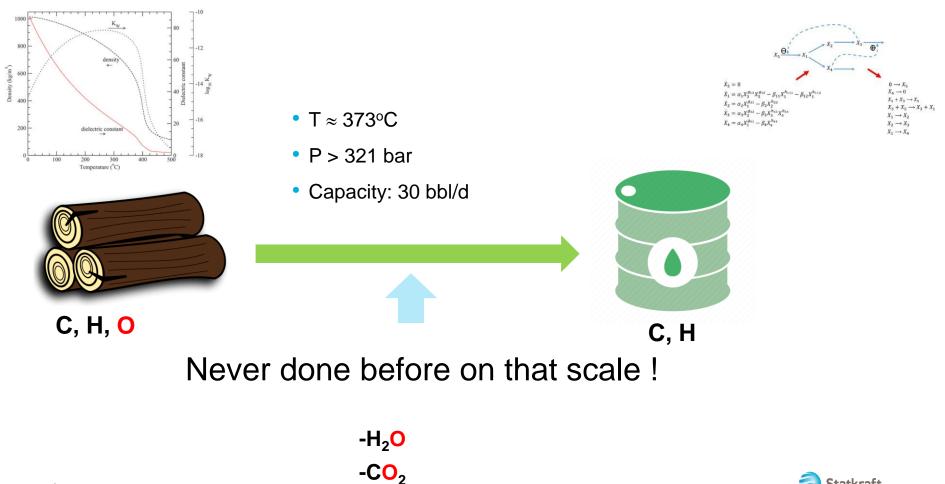


Silva Green Fuel

Key milestones since established in 2015



HTL: Challening the unkown





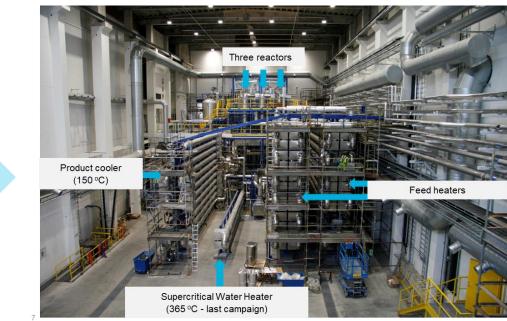
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HTL-demo Tofte: world-wide 1st of its kind (5 t/d)

PURPOSE

- De-risking
- Testing core technology
- Basis for Scale up
- System integration
- Selection of materials
- Handling of side-streams
 and water

Scale-up: X 100



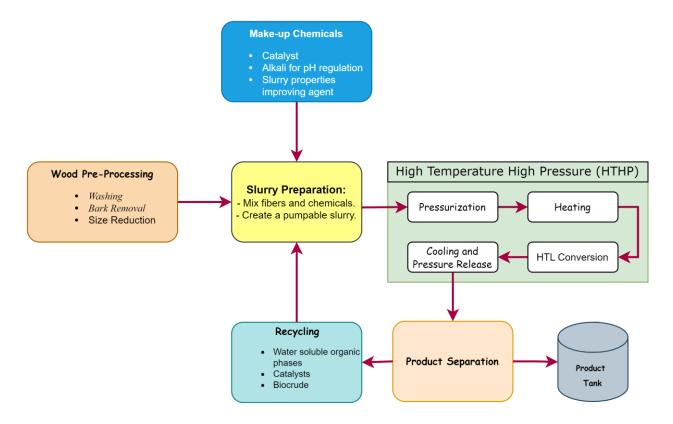




Technology provider`s pilot plant in Aalborg

Statkraft Internal

HTL at SGF Demo plant in Tofte





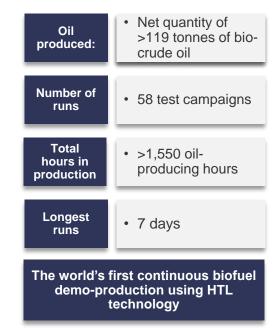
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Demo-plant set-up: mini "full-scale" plant



• The demo-plant is set-up like a "full-scale" operation including all relevant side streams and processes you would have in a full-scale production, including a control room providing 24/7 observation and surveillance

Key operational KPIs¹):





1) KPIs as of June 2024

Experiences Gained Operating the Demo Plant

Positive Findings

Proof of wood conversion chips to high quality oil

Able to tune oil quality by operating parameters

Demonstration in operational environment (TRL7) of several specially designed systems

Technical issues solved

Leakages in high pressure seals

High pressure slurry pump

Pumping of main and intermediate products

Interphase detection in oil/water separators

Tuning of thermal oxidizer

Major Process related Set-backs

Corrosion findings

Fouling of high temp conversion equipment

Other learnings

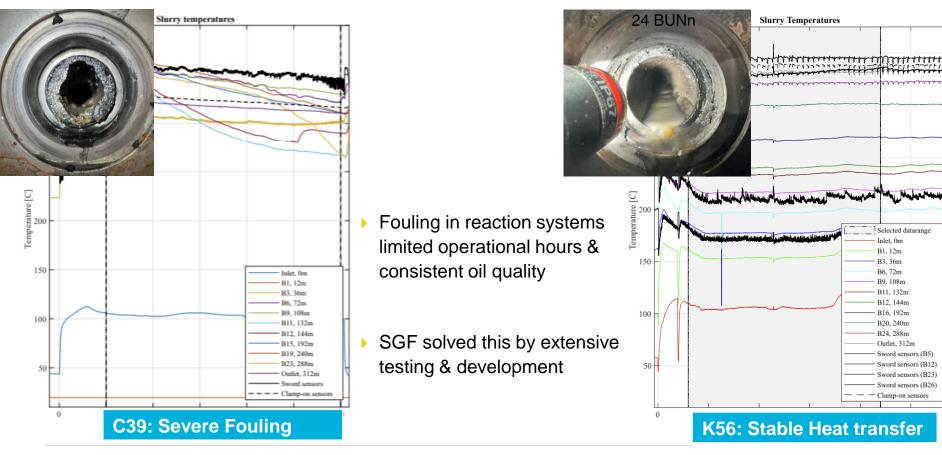
HSE activities for a HTHP chemical plant

Operator training of 5 shifts

Fixation of operating parameters during test campaigns



Major Process Related Setbacks (I): Fouling

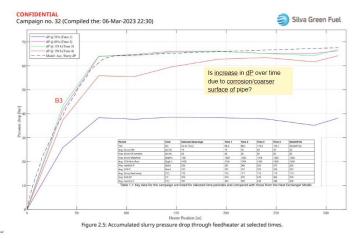




Major Process Related Setbacks (II) - Corrosion

- Pipe Rupture in in HP feedheater system
- Significant material loss through Corrosion in first part of FH
- Erosion-Corrosion mechanism: Solid particles (biomass, coke, salts), corrodents (acetates, formats, CO2, chlorides..)
- Construction Material P91 steel not appliable
- Critical part (first 65 meters) now replaced with resistant material
- First campaign with new HX system successful (no corrosion detected)







SGF Demo Plant at a Glance

- > SGF is steadily solving the issues by dedicated development
- > Next milestone: 1000h campaign







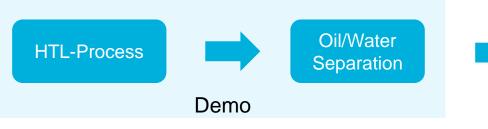


Demo Plant Figures





Upgrading of HTL biocrude





In collaboration with external partner

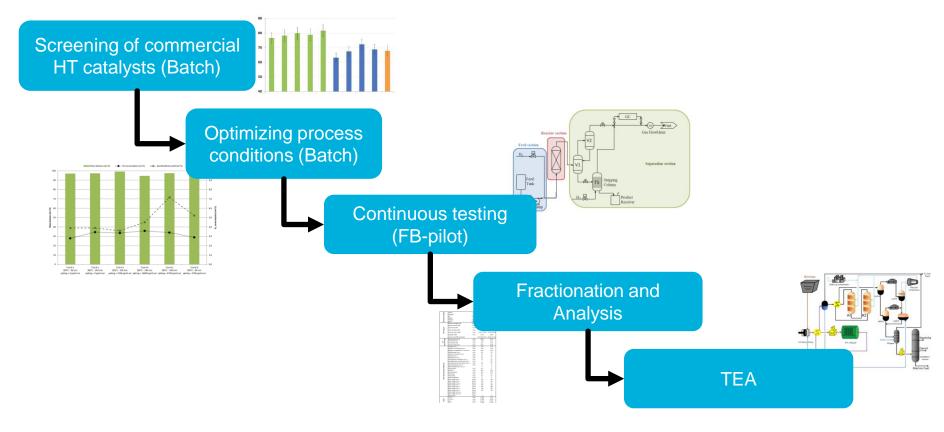
Analysis	Unit	P0254 washed (biocrude Nov 2020)
Water	wt%	0.65
Density @15°C from calculation	kg/m3	1083
Density @70°C from measurement	kg/m5	1046
Kinematic Viscosity @ 20°C		
Kinematic Viscosity @ 40°C]	
Kinematic Viscosity @ 50°C	cSt	3740
Kinematic Viscosity @ 70°C		
Kinematic Viscosity @ 100°C		70
Carbon	wt% (wet basis	79.9
Hydrogen	wt% (wet basis	8.66
Oxygen	wt% (wet basis	11.36
Nitrogen	wt% (wet basis	0.0905
Sulfur	wt% (wet basis	0.0147
Metals	wt% (wet basis	0.0317
Total CHONS + metals	wt% (wet basis	100.1
Distillation yields		
IP-180°C (aqueous phase)	wt%	1.0
IP-180°C (organic phase)	wt%	0.9
180-350°C	wt%	29.2
350°C+	wt%	68.9
NMR 13C		
Carboxyl or carbonyl bond	wt%	3
Aromatic C-O bond	wt%	7
Aromatic C-C bond	wt%	24
Aromatic C-H bond	wt%	15
Methoxyl-Aromatic bond	wt%	0
Aliphatic C-C bond	wt%	51



Continuous demineralization process verified on Lab-scale & Pilotscale



Upgrading: Development Method





Promising results from continuous pilot-scale upgrading

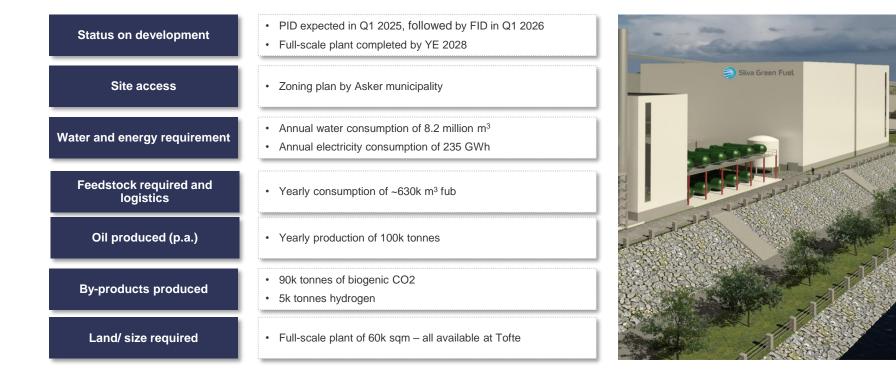


1200 hrs cont operation	(HTL-oil)
▶ Wt% O: < 0.1 %	(11.4)
D15 = 0.9001 kg/l	(1.083)
► H/C = 1.62	(1.30)

Boiling Range [ºC]	Cut	Wt%
C5-180	Naphtha	15
180-350	Middle Distillate	57
350-540	Vacuum Gas Oil	23
540+	Vacuum Residue	5



SGF – Strong business case for first commercial plant





Thank you for your attention !



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